



INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification ⁶ : C07C 17/278, 19/10, 19/14, 17/23	A1	(11) International Publication Number: WO 95/16655 (43) International Publication Date: 22 June 1995 (22.06.95)
(21) International Application Number: PCT/US94/14367 (22) International Filing Date: 13 December 1994 (13.12.94) (30) Priority Data: 08/166,431 14 December 1993 (14.12.93) US (71) Applicant: E.I. DU PONT DE NEMOURS AND COMPANY [US/US]; 1007 Market Street, Wilmington, DE 19898 (US). (72) Inventors: SIEVERT, Allen, Capron; 215 Rhett Lane, Elkton, MD 21921-2059 (US). NAPPA, Mario, Joseph; 3 Oakridge Court, Newark, DE 19711-3435 (US). (74) Agents: BOYER, Michael, K. et al.; E.I. du Pont de Nemours and Company, Legal/Patent Records Center, 1007 Market Street, Wilmington, DE 19898 (US).		(81) Designated States: JP, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE). Published <i>With international search report.</i> <i>Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i>
(54) Title: PROCESS FOR FLUORINATED PROPANES AND PENTANES (57) Abstract The instant invention relates to producing fluorinated propanes and pentanes. More particularly it relates to producing perhalofluoropropanes and pentanes by reacting dihalodifluoromethanes with polyfluoroethylenes, notably tetrafluoroethylene (TFE) and chlorotrifluoroethylene (CTFE) while in the presence of an aluminum chlorofluoride catalyst.		

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TITLE

PROCESS FOR FLUORINATED PROPANES AND PENTANES

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FIELD OF THE INVENTION

The instant invention relates to producing fluorinated propanes and pentanes. More particularly it relates to producing perhalofluoropropanes and pentanes by reacting dihalodifluoromethanes with polyfluoroethylenes, notably tetrafluoroethylene (TFE) and chlorotrifluoroethylene (CTFE) while in the presence of an aluminum chlorofluoride catalyst.

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In another aspect, the instant invention relates to preparing novel perbromofluoroalkanes containing three, or five carbon atoms.

In still another aspect, the instant invention relates to a process for converting the perhalofluorocarbons to hydrofluorocarbons (HFCs) by reaction with a source of active hydrogen effective to convert one or more carbon-nonfluorohalogen bonds to carbon-hydrogen bonds.

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Thus, the perhalofluoropropanes and pentanes, products of the inventive process, are potentially useful for manufacturing hydrofluorocarbons which, in turn, in view of their inherently low ozone depletion potentials, are environmentally attractive alternatives for perchlorofluorocarbons (CFC's) in such established uses as refrigerants, expansion agents, aerosol, propellants, fire extinguishing agents, power cycle working fluids, polymerization media, heat transfer media, solvents, carrier fluids, cleaning and drying agents, gaseous dielectrics, among other applications.

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BACKGROUND OF THE INVENTION

Joyce, U. S. Patent No. 2,462,402 (Feb. 22, 1949) discloses a process for the production of highly halogenated fluoroalkanes which comprises contacting TFE with a polyhalogenated alkane, preferably a methane, containing at least one chlorine atom and no more than two fluorine atoms, in the presence of a polyvalent metal halide catalyst, preferably aluminum chloride.

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U. S. Patent No. 2,462,402, to Coffman, et. al., is referenced in the Journal of the American Chemical Society, Vol. 71, pages 979-980 (1949) which discloses that reacting CHClF_2 (chlorodifluoromethane) while in the presence of aluminum chloride with TFE produces CHCl_2F_5 having one less F atom than the

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5 sum of fluorine atoms in the reactants. Likewise, CHClF_2 reacting with CTFE yields CHCl_3F_4 .

Paleta, in a review article "Fluorine Chemistry Reviews", Vol. 8, page 51 (1977) states: "The ionic addition reactions of fluoromethanes in the presence of aluminum chloride are limited to the monofluoro derivatives only. When in contact
10 with aluminum chloride, both difluorodichloromethane and difluorochloromethane were found to undergo a rapid disproportionation with the formation of monofluorochloromethanes (along with some further compounds) that are able to add to fluoroethylenes."

The disclosure of each of the previously identified references is
15 hereby incorporated by reference.

SUMMARY OF THE INVENTION

One aspect of this invention relates to a process for producing valuable perhalopolyfluoropropanes and pentanes from known
20 dihalodifluoromethanes, particularly dichlorodifluoromethane, and polyfluoroethylenes, such as tetrafluoroethylene (hereinafter referred to as "TFE") and chlorotrifluoroethylene (hereinafter referred to as "CTFE").

Another aspect of the invention provides such a process that produces propanes and pentanes wherein the total number of fluorine atoms is equal to the
25 sum of the number of fluorine atoms in the dihalodifluoromethane reactant and the number of fluorine atoms in the polyfluoroethylene reactant.

Still another aspect of the invention relates to novel perbromofluoropropanes and pentanes.

A still further aspect of the invention relates to a process for obtaining
30 hydropolyfluoropropanes and pentanes having relatively low ozone depletion potentials wherein carbon-nonfluorohalogen bonds, e.g., C-Cl or C-Br bonds, of the perhalofluoropropanes and pentanes are converted to carbon-hydrogen bonds.

Notwithstanding conventional beliefs as described in Paleta, the instant invention can react dihalodifluoromethanes, wherein the halo corresponds to
35 non-fluoro halogens, with TFE and/or CTFE to produce perhalofluoropropanes and/or pentanes, wherein the total number of fluorines in said propanes and pentanes is equal to the sum of the fluorines in the methanes and fluoroolefins being reacted.

The process of the invention comprises producing
40 perhalofluoropropanes and/or pentanes by:

5 (i) contacting (a) a dihalodifluoromethane, $CXYF_2$, wherein X and Y are independently Cl or Br, with (b) at least one of tetrafluoroethylene and chlorotrifluoroethylene while in the presence of (c) a catalytic amount of an effective aluminum chlorofluoride, at a temperature and pressure effective to result in the formation of (d) at least one of a perhalofluoropropane having 5 to 6 fluorine
10 atoms and 2 to 3 nonfluorohalogen atoms, e.g., bromine and/or chlorine atoms, and a perhalofluoropentane having 8 to 10 fluorine atoms and 2 to 4 nonfluorohalogen atoms, e.g., bromine and/or chlorine atoms; the total number of fluorine atoms in said propane and/or pentane products being the sum of the number of fluorine atoms in the dihalodifluoromethane and the number of fluorine atoms in the TFE
15 and/or CTFE, and;

(ii) recovering at least one of said propanes and pentanes.

In one aspect of the invention, the dihalodifluoromethane comprises CCl_2F_2 (CFC-12), the fluoroethylene comprises TFE and the aluminum chlorofluoride contains about 3 to about 64% F by weight, normally about 16 to 61
20 % F by weight. Such aluminum chlorofluorides, which correspond to $AlCl_{3-x}F_x$, wherein x is typically about 1.0 to about 2.8, are hereinafter referred to as "modified aluminum chlorides". Modified aluminum chlorides are conveniently prepared by reacting commercially available anhydrous $AlCl_3$ with one or more chlorofluorocarbons, hydrochlorofluorocarbons, or hydrofluorocarbons as disclosed
25 in U.S. Patent No. 5,157,171 to Sievert, et. al. at column 4 line 2 through column 5 line 4, the entire disclosure of which is hereby incorporated herein by reference.

In one embodiment of the invention, the reaction conditions, e.g., the mole ratios of reactants, their feed rates, and temperature and pressure, are controlled so as to favor a one-to-one reaction of the dihalodifluoromethane with
30 the fluoroolefin, while in the presence of a modified aluminum chloride catalyst, and result in the formation of halofluoropropanes as the predominant products as illustrated by equation (1).



In another embodiment, the reaction conditions are adjusted for
35 promoting production of halofluoropentanes as the predominant products via a one-to-two reaction stoichiometry, while in the presence of a modified aluminum chloride catalyst, as illustrated in equation (2).



In still another aspect of the invention, the reaction products, as
40 perhalofluoropropanes and/or as perhalofluoropentanes are treated with one or

- 5 more reducing means under conditions effective for converting the non-fluorohalide groups of the propanes and pentanes, i.e., the -CXY- groups, wherein X and Y are independently Cl or Br, to -CHX- or -CH₂- groups, usually the latter. The reducing means include photochemical reducing means, chemical reducing means, catalytic hydrogenation reducing means, among other suitable means.

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DETAILED DESCRIPTION

In accordance with the present invention one or more perhalofluoropropanes comprising (A) C₃X₂YF₆, when produced from TFE, (B) C₃ClX₂YF₅, when produced from CTFE, and perhalofluoropentanes having the
 15 formula C₅X₂YF₁₀, when produced from TFE, (C) C₅Cl₂X₂YF₈, when derived from a mixture of TFE and CTFE; wherein X and Y stand for Cl or Br as defined above, can be prepared by reacting CXYF₂, e.g., CCl₂F₂, with TFE and/or CTFE in the presence of a modified aluminum chloride catalyst. The reactions may be represented by equations (1) and (2) above, illustrated with CCl₂F₂ and TFE as the
 20 reactants.

The CXYF₂ starting materials for the process of this invention can be selected from at least one member selected from the group of CCl₂F₂, CBrClF₂, and CBr₂F₂. The fluoroolefin starting materials for the process of this invention are selected from one or more of CTFE (CClF=CF₂) and TFE (CF₂=CF₂). The
 25 combination of these CXYF₂ starting materials with these fluoroolefin starting materials in the presence of a modified aluminum chloride catalyst permits making reaction products selected from one or more of C₃Cl₄F₄ isomers including CCl₃CF₂CClF₂ and CCl₃CClF₂CF₃; C₃BrCl₃F₄ isomers including CCl₂FCF₂CBrClF; C₃Br₄F₄ isomers including CBr₃CF₂CBrF₂; C₃Cl₃F₅ isomers including CCIF₂CCl₂CF₃, CCIF₂CClFCClF₂, CCl₂FCClF₂CF₃, CCl₂FCF₂CClF₂, and CCl₃CF₂CF₃; C₃BrCl₂F₅ isomers including CF₃CBrClCClF₂, CCIF₂CF₂CBrClF, CCIF₂CClF₂CBrF₂, CBrCl₂CF₂CF₃ and CBrF₂CF₂CCl₂F; C₃Br₂ClF₅ isomers including CBr₂ClCF₂CF₃; C₃Br₃F₅ isomers including CBr₃CF₂CF₃ and CBrF₂CBr₂CF₃; C₃Cl₂F₆ isomers, including CCl₂FCF₂CF₃ and CCIF₂CF₂CClF₂; C₃BrClF₆ isomers, including CBrClF₂CF₂CF₃, CBrF₂CF₂CClF₂, and CF₃CBrClCF₃; C₃Br₂F₆ isomers, including CBr₂FCF₂CF₃, CBrF₂CF₂CBrF₂, and CF₃CBr₂CF₃; C₅Cl₄F₈ isomers, including CF₃CClFCCl₂CClF₂CF₃, CCIF₂CClF₂CF₂CCl₂CF₃, and CCIF₂CF₂CCl₂CF₂CClF₂; C₅BrCl₃F₈ isomers; C₅Br₂Cl₂F₈ isomers; C₅Cl₃F₉ isomers including
 35 CCIF₂CF₂CCl₂CF₂CF₃, C₅BrCl₂F₉ isomers; C₅Br₂ClF₉ isomers; C₅Br₃F₉ isomers

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- 5 including CBrF₂CF₂CBr₂CF₂CF₃; C₅Cl₂F₁₀ isomers including C₂F₅CCl₂C₂F₅ and CF₃CCl₂CF₂CF₂CF₃; C₅BrClF₁₀ isomers including C₂F₅CBrClC₂F₅ and CF₃CBrClCF₂CF₂CF₃; and C₅Br₂F₁₀ isomers including C₂F₅CBr₂C₂F₅ and CF₃CBr₂CF₂CF₂CF₃.

Novel perhalofluoropropanes and pentanes that can be produced by
10 using the inventive process comprise at least one member from the group of
CClF₂CF₂CBrClF, CBrCl₂CF₂CF₃ and CBrF₂CF₂CCl₂F; CBr₃CF₂CF₃ and
CBrF₂CBr₂CF₃; CClF₂CClF₂CF₂CCl₂CF₃ and CClF₂CF₂CCl₂CF₂CClF₂;
C₅Br₂Cl₂F₈ isomers; CClF₂CF₂CCl₂CF₂CF₃, C₅BrCl₂F₉ isomers; C₅Br₂ClF₉
isomers; CBrF₂CF₂CBr₂CF₂CF₃; C₂F₅CCl₂C₂F₅ and CF₃CCl₂CF₂CF₂CF₃;
15 C₂F₅CBrClC₂F₅ and CF₃CBrClCF₂CF₂CF₃; C₂F₅CBr₂C₂F₅ and
CF₃CBr₂CF₂CF₂CF₃. Such novel perhalofluoroalkanes can be used for making
useful hydrofluorocarbons (HFCs) such as hydrofluoropropanes and
hydrofluoropentanes. Such HFCs can be used as refrigerants, blowing agents,
cleaning compositions, among other applications.

20 The process of equation (1) indicates a stoichiometry of one mole of
CXYF₂ per mole of TFE (or CTFE); however, an excess of either reactant may be
used as desired with excess of the fluoroolefin promoting formation of the C₅
product. Even at mole ratios of about 1:1 however, significant quantities of C₅-
product can be produced (equation (2)) along with C₃-product (equation (1)). The
25 relative proportions of the two reactants can be varied widely for producing a
desired product or product mixture of products.

Generally, the mole ratio may vary from about 3 to 1 moles of CXYF₂
component per mole of the fluoroolefin, to promote C₃ production and from about
3 to 1.5 moles of the fluoroolefin per mole of the CXYF₂ to promote C₅
30 production.

In some cases, CCl₂F₂ may also be employed in the formation of
modified aluminum chloride, as defined above, use of sufficient excess enables the
production of modified aluminum chloride in situ from anhydrous aluminum
chloride so that the catalyst modification reaction need not be carried out as a
35 separate step. The ability to form the modified catalyst in situ constitutes an
improvement over the art because the process can be practice by using AlCl₃
thereby obviating a modified catalyst formation step. It is, however, important that
the excess quantity, for example, of CCl₂F₂, avoids converting the AlCl_x-3F_x to
AlF₃ which in turn can adversely effect the inventive process. In some cases, the
40 CCl₂F₂ and TFE and/or CTFE can be simultaneously contacted with the AlCl₃.

5 The process can be conducted batchwise or in a continuous manner.
In the continuous mode, a mixture of dihalodifluoromethane and fluoroolefin is
passed through or over a bed or body of modified aluminum chloride which may be
under agitation at suitable temperature and pressure to form a product stream, and
the desired products are recovered from the stream by conventional methods such
10 as fractional distillation. In some cases, the reactants can be added individually or
simultaneously.

In the batch process, the reactants and catalyst may be combined in a
suitable commercially available reactor to form a reaction mixture and the mixture
held at a suitable temperature and pressure, normally under agitation, until a
15 desired degree of conversion to the desired propanes and/or pentanes is attained.
In one embodiment, the reactor is initially charged with the catalyst, and optionally
with a diluent, then the dihalodifluoromethane and the fluoroolefin, as separate
streams or as a combined stream, in a desired mole ratio, are fed into the reactor at
a controlled rate and maintained therein until the reaction is substantially complete.
20 If the reactor is fed with dihalodifluoromethane and catalyst in the substantial
absence of fluoroolefin, then the system (reactor and ingredients) should be kept
relatively cold, e.g., between about -78C and 10C, to minimize disproportionation of
the dihalodifluoromethane to higher and lower fluorine content methanes.

The process may be practiced with or without a solvent or reaction
25 diluent. Such material, if used, must be substantially inert to the reactants and
catalyst, and also should boil at a temperature enabling separation from the propane
and pentane reaction products. Representative of such solvents comprise at least
one member from the group of CCl₄, CF₃CHCl₂, CCl₃CF₃, propane and pentane
products of the present invention process, e.g., CF₃CF₂CCl₂F, CClF₂CF₂CClF₂,
30 CF₃CF₂CCl₂CF₂CF₃, CF₃CCl₂CF₂CF₂CF₃, and isomers, among others.

The reaction temperature may be varied, and normally is in the range
of from about 0C to about 150C, usually in the range of from about 20C to about
110C.

The reaction pressure likewise may vary widely from subatmospheric
35 to superatmospheric; but normally the reaction is carried out at elevated pressures,
particularly at pressures generated autogenously in conformity with the reaction
temperature employed. The pressure may be controlled by adjusting the amount of
unreacted dihalodifluoromethane and fluoroolefin.

The reaction time, or time necessary for sufficient substantially
40 complete reaction, can vary with the temperature chosen for the reaction. In

5 general the higher the temperature the shorter the reaction time. The degree of
reaction, however, is easily determined by the change in the autogenous pressure in
the reaction vessel, because the pressure drops as the reaction proceeds, so that the
time at which the pressure stops decreasing can be taken as the end of the reaction
period. The reaction time can also vary with the quantity or volume of reactants in
10 the reactor. Generally, the reaction time, is in the range of from about 0.25 h to
about 8.0 hours are normally employed temperature ranges.

 The amount of modified aluminum chloride generally employed is in
the range of from about 1 to 20 percent based on the weight of the
dihalodifluoromethane reactant.

15 The reaction products may be recovered from the reactor by using any
suitable conventional means such as by filtration or distillation. It is usually
convenient to decompose the catalyst by treatment with water and then recover the
product by distillation.

 If desired, the perhaloproducts of the invention process may be
20 hydrodehalogenated to hydro-derivatives comprising at least one hydrogen
substituent and correspondingly one less nonfluorohalogen substituent than present
in the starting perhalofluorocarbon by being treated with one or more reducing
means. Examples of suitable reducing means comprise at least one of
photochemical, chemical, and normally catalytic hydrogenation means. Catalytic
25 hydrogenation may generally be effected with molecular hydrogen over a suitable
catalyst, typically a Group VIII metal, as disclosed, for example, in Smith, U. S.
Patent No. 2,942,036 and Rao, U. S. Patent No. 5,136,113; the entire disclosures of
which are incorporated herein by reference.

 Catalytic hydrogenation can be practiced in the liquid or vapor phase.
30 Normally, the vapor phase is employed with a catalytic metal such as palladium that
can be supported on carbon or alumina; usually the latter. Catalytic hydrogenation
may generally be effected with molecular hydrogen over a suitable catalyst, typically
a Group VIII metal, as disclosed, for example, in Smith, U. S. Patent 2,942,036 and
Rao, U. S. Patent 5,136,113 which disclosures are incorporated herein by reference.

35 Hydrogenation can also be conducted in the vapor phase with a
catalytic metal such as nickel, palladium, platinum, rhodium, iridium, among others.
The catalytic metal is normally supported on a suitable carrier such as carbon or
alumina. The use of alumina as a support for palladium is particularly desirable for
hydrodechlorination and hydrodebromination as illustrated in Example 22 for the
40 conversion of $\text{CF}_3\text{CF}_2\text{CCl}_2\text{CF}_2\text{CF}_3$ to $\text{CF}_3\text{CF}_2\text{CH}_2\text{CF}_2\text{CF}_3$. The use of carbon as

5 a support for palladium is effective for hydrogenating, when a combination of hydrodehalogenation, dehydrofluorination, and hydrogen addition is desired as illustrated in Examples 20 and 21 for the conversion of $\text{CF}_3\text{CF}_2\text{CCl}_2\text{CF}_2\text{CF}_3$ to $\text{CF}_3\text{CHFCH}_2\text{CF}_2\text{CF}_3$.

10 The hydrodehalogenation reactions of the present invention may be conducted at temperatures between about 25C and 250C, normally between about 50C and 200C, and typically between about 100C and 200C. The choice of optimum hydrodehalogenation temperature will be dictated by whether the halogen being removed or replaced is chlorine or bromine, the desired degree of conversion of the perhalofluoroalkane starting material, the percent loading of the active metal upon
15 the support, among other factors. Perbromofluoroalkanes are more readily hydrodehalogenated than are perchlorofluoroalkanes.

The hydrodehalogenation reactions may be operated at pressures between atmospheric and 100 psig or higher. The choice of pressure may be dictated by the vapor pressure of the reactants, intermediates, and products.

20 The ratio of hydrogen to perhalofluoroalkane employed in the dehydrohalogenation reaction may vary from about 0.5 to about 10 on a molar basis, and usually should be from about 1 to 4. Relatively large excesses of hydrogen can be employed. A deficiency of hydrogen may be used to control the conversion rate of the perhalofluoroalkane if desired.

25 The products of the hydrodehalogenation reaction may be separated from excess hydrogen, if any, and HF, HCl, and/or HBr by-products by normal distillation or neutralization techniques. The products of the hydrodehalogenation comprise at least one member from the group of hydrofluoroalkanes, hydrofluoroalkenes, hydrohalofluoroalkanes, and hydrohalofluoroalkenes.

30 Examples of hydrodehalogenation products from the hydrodechlorination of $\text{CF}_3\text{CF}_2\text{CCl}_2\text{CF}_2\text{CF}_3$ (see Examples 20, 21, and 22) comprise at least one of $\text{CF}_3\text{CF}_2\text{CH}_2\text{CF}_2\text{CF}_3$, $\text{CF}_3\text{CHFCH}_2\text{CF}_2\text{CF}_3$, $\text{CF}_3\text{CF}=\text{CHCF}_2\text{CF}_3$, $\text{CF}_3\text{CF}_2\text{CHClCF}_2\text{CF}_3$, $\text{CF}_3\text{CF}=\text{CClCF}_2\text{CF}_3$, among others.

The hydrohalofluoroalkanes, hydrofluoroalkenes, and
35 hydrohalofluoroalkenes are intermediates in the formation of the hydrofluoroalkanes and may be separated from the hydrofluoroalkanes for conversion to the saturated products.

Hydrofluoropropanes and hydrofluoropentanes produced by hydrodehalogenation of the perhalofluoroalkanes comprise at least one of $\text{C}_3\text{H}_4\text{F}_4$
40 isomers including $\text{CH}_3\text{CF}_2\text{CHF}_2$, $\text{CH}_3\text{CHFCH}_2\text{F}$, and $\text{CH}_2\text{FCF}_2\text{CH}_2\text{F}$; $\text{C}_3\text{H}_3\text{F}_5$

5 isomers including CHF₂CH₂CF₃, CHF₂CHFCHF₂, CH₂FCHFCF₃,
 CH₂FCF₂CHF₂, and CH₃CF₂CF₃; C₃H₂F₆ isomers including CH₂FCF₂CF₃,
 CHF₂CF₂CHF₂, and CF₃CH₂CF₃; C₅H₈F₄ isomers including
 CHF₂CH₂CH₂CH₂CHF₂; C₅H₇F₅ isomers including CHF₂CH₂CH₂CH₂CF₃,
 and CHF₂CHFCH₂CH₂CHF₂; C₅H₆F₆ isomers including CF₃CH₂CH₂CH₂CF₃,
 10 CHF₂CH₂CHFCH₂CF₃, CHF₂CHFCH₂CH₂CF₃, and CHF₂CF₂CH₂CH₂CHF₂;
 C₅H₅F₇ isomers including CF₃CH₂CH₂CHF₂CF₃, CHF₂CHFCHFCH₂CF₃,
 CHF₂CF₂CH₂CHFCHF₂, CHF₂CF₂CH₂CH₂CF₃, and CHF₂CH₂CH₂CF₂CF₃;
 C₅H₄F₈ isomers including CF₃CHFCH₂CHF₂CF₃, CHF₂CHF₂CH₂CF₃,
 CHF₂CF₂CH₂CF₂CHF₂, CHF₂CF₂CH₂CHF₂CF₃, CF₃CH₂CH₂CF₂CF₃, and
 15 CHF₂CHFCH₂CF₂CF₃; C₅H₃F₉ isomers including CF₃CHFCH₂CF₂CF₃,
 CF₃CH₂CHF₂CF₂CF₃, and CHF₂CF₂CH₂CF₂CF₃; C₅H₂F₁₀ isomers including
 C₂F₅CH₂C₂F₅ and CF₃CH₂CF₂CF₂CF₃.

Novel hydrofluoroalkanes comprise at least one member from the
 group consisting of CHF₂CH₂CH₂CH₂CHF₂; CHF₂CH₂CH₂CH₂CF₃ and
 20 CHF₂CHFCH₂CH₂CHF₂; CHF₂CH₂CHFCH₂CF₃, CHF₂CHFCH₂CH₂CF₃, and
 CHF₂CF₂CH₂CH₂CHF₂; CF₃CH₂CH₂CHF₂CF₃, CHF₂CHFCHFCH₂CF₃,
 CHF₂CF₂CH₂CHFCHF₂, CHF₂CF₂CH₂CH₂CF₃, and CHF₂CH₂CH₂CF₂CF₃;
 CF₃CHFCH₂CHF₂CF₃, CHF₂CHF₂CH₂CF₃, CHF₂CF₂CH₂CF₂CHF₂,
 CHF₂CF₂CH₂CHF₂CF₃, and CHF₂CHFCH₂CF₂CF₃;
 25 All of the above hydrofluoroalkanes can be used in the manner described above in
 connection with HFCs such as refrigerants, blowing and cleaning agents, among
 other applications.

In addition to hydrogenation, suitable chemical reducing means that
 may be used include reducing with zinc in the presence of an alcohol as disclosed,
 30 for example, by Morikawa, et. al., in International Patent Application 90/08753, and
 by Krespan in U. S. Patent No. 4,935,558; reduction with a complex metal hydrides
 as disclosed by Clayton in European Patent Application Publication No. 0 508,631;
 reduction with hydrogen iodide or with H₂ in the presence of iodine or hydrogen
 iodide as disclosed by Anton in U. S. Patent No. 5,208,396; the entire disclosure of
 35 which are hereby incorporated herein by reference.

Suitable photochemical reducing means include reaction of the
 perhalocompound with alcohols in the presence of ultraviolet light as disclosed by
 Posta, et. al., in Czechoslovak Patent No. 136,735.

5 The various aspects of this invention may are more readily understood by reviewing the following examples that are provided to illustrate not limit the scope of the appended claims.

 Examples 1 to 7 illustrate reacting CCl_2F_2 (CFC-12) with $\text{CF}_2=\text{CF}_2$ (TFE) catalyzed by separately prepared modified aluminum chloride catalyst while
10 Example 8 utilizes initially unmodified AlCl_3 as the catalyst.

 Examples 8 to 16 utilize CBrClF_2 and CBr_2F_2 as the dihalodifluoromethane reactant, with Example 16 showing the effect of using initially unmodified AlCl_3 as the catalyst.

 Examples 17 to 19 illustrate the use of $\text{CClF}=\text{CF}_2$ (CTFE) in place of
15 TFE.

 Examples 20-22 illustrate preparing hydrofluorocarbons from perhalofluoropropanes and pentanes utilizing catalytic hydrogenation.

 Analyses of reaction products, generally mixtures, were carried out using standard GC/GC-MS and ^{19}F NMR methods, the abbreviations GC, GC-MS, and NMR standing for gas chromatography, gas chromatography-mass
20 spectrometry, and nuclear magnetic resonance spectroscopy. Results are presented in GC area percents unless otherwise indicated with amounts less than about 1% generally omitted.

25

EXAMPLE 1

Reaction of CFC-12 with Tetrafluoroethylene

 A 400 mL "Hastelloy" C shaker tube was charged with CCl_3F -modified aluminum chloride (3.0 g). The tube was sealed, cooled to -78°C , evacuated, and purged with nitrogen three times.

30 The reactor was then charged with CCl_2F_2 (50 g, 0.41 mole). The cold reactor was placed in the barricaded enclosure, and charged with 25 g (0.25 mole) of TFE. The reactor was warmed to 60°C over the course of 0.25 h; during this time the pressure rose to 80 psig. The temperature was held at 60°C for 1.3 h (pressure = 80-85 psig) and then raised to 80°C and held for 1 h (pressure = 112-116
35 psig). The following day the reactor was discharged to afford 54.7 g of a clear supernatant over a brown solid. Analysis of the product by GC/GC-MS and ^{19}F NMR indicated the following composition:

5	<u>Component</u>	<u>GC Area %</u>	<u>Mole %</u>
	CCl ₂ F ₂	1.3	-
	CCl ₂ FCF ₂ CF ₃	68.5	53.5
	CClF ₂ CF ₂ CClF ₂	*	13.9
	CCl ₃ F	0.1	-
10	C ₂ F ₅ CCl ₂ C ₂ F ₅	26.5	29.8
	CCl ₃ CF ₂ CF ₃	2.1	2.8
	CCl ₂ FCF ₂ CClF ₂	0.2	-
	CCl ₄	0.8	-

*C₃Cl₂F₆ isomers were not separated by GC.

15

Noteworthy are the substantial yields of the hexafluorides, CCl₂FCF₂CF₃ and CClF₂CF₂CClF₂, and the decafluoride, CF₃CF₂CCl₂CF₂CF₃. Also, the appearance of CCl₃F and CCl₄ along with the pentafluorides, CCl₃CF₂CF₃ and CCl₂FCF₂CClF₂, probably derived therefrom, indicates some

20 disproportionation of the starting CFC-12 reactant had occurred.

The modified aluminum chloride catalyst of Example 1 was prepared as follows:

A 500 mL three neck round bottom flask containing a PTFE-coated stirring bar was charged with 50 g of aluminum chloride (AlCl₃) in a dry box. The

25 flask was passed out of the dry box and fitted with an addition funnel and a dry ice condenser connected to a nitrogen bubbler. The addition funnel was charged with 175 mL of CCl₃F and the condenser was filled with a methanol/dry ice mixture. The CCl₃F was gradually added to the flask and the mixture began to reflux vigorously. The reaction continued to reflux for a hour after all of the CCl₃F had

30 been added. The reaction was not heated. GC analysis of the supernatant liquid indicated it was essentially pure CCl₄. The mixture was stirred overnight at ambient temperature and then volatiles were removed in vacuum. The resulting solid was dried under dynamic vacuum to afford 22 g of off-white powder. Analysis: weight % F = 57.8; this corresponds to a composition that is approximately AlCl_{0.3}F_{2.7}.

35

EXAMPLE 2

Reaction of CFC-12 with Tetrafluoroethylene

A 400 mL "Hastelloy" C shaker tube was charged with CCl₃F-modified aluminum chloride (1.5 g). The reactor was sealed, cooled to -78C,

40 evacuated, and purged with nitrogen three times. The reactor was then charged with

5 CCl₂F₂ (40 g, 0.33 mole). The cold reactor was placed in the barricade and charged with 15 g (0.15 mole) of TFE. The reactor was warmed to 30C over the course of 0.5 h and the pressure rose to 40 psig. TFE was then added to the reactor in 5 g increments at a temperature of 31-32C until a total of 50 g (0.50 mole) had been added; the pressure gradually rose to 114 psig. The reactor was then held at a
 10 temperature 31-2C for 3 h; the final pressure was 59 psig. The following day the reactor was discharged to afford 54.7 g of a clear supernatant over a brown solid. Analysis of the product by GC/GC-MS and ¹⁹F NMR indicated the following composition:

15	<u>Component</u>	<u>GC Area %</u>
	CClF ₂ CF ₂ ClF ₂ /CCl ₂ FCF ₂ CF ₃	12.6
	CF ₃ CCl ₂ CF ₂ CF ₂ CF ₃	.0
	CF ₃ CF ₂ CCl ₂ CF ₂ CF ₃	83.7
	C ₃ Cl ₃ F ₅ isomers	1.0
20	C ₅ Cl ₃ F ₉ isomers	0.9

The modified aluminum chloride catalyst of Example 2 was prepared following a procedure similar to that described in Example 1 except that the reaction volatiles were removed promptly after the reaction ceased to reflux.

25 Analysis: weight % F = 47.7; weight % Al = 26.6; this corresponds to a composition that is approximately AlClF₂.

EXAMPLE 3

Reaction of CFC-12 with Tetrafluoroethylene

30 A 400 mL "Hastelloy" C shaker tube was charged with CCl₃F- modified aluminum chloride (4 g) and 128 g of CCl₃CF₃ as a diluent. The reactor was sealed, cooled to -78C, evacuated, purged with nitrogen three times, and charged with CCl₂F₂ (50 g, 0.41 mole). The cold reactor was placed in the barricade and charged with 20 g (0.20 mole) of TFE. The reactor was warmed to
 35 30C over the course of 0.25 h and the pressure rose to 45 psig. TFE was then added to the reactor in 5 g increments at a temperature of 29-30C over the next 1.5 h until a total of 50 g (0.50 mole) had been added; the pressure gradually rose to 42 psig. The reactor was then held at a temperature 30C for 3 h; the final pressure was 20 psig. The following day the reactor was discharged to afford 228.1 g of a clear

- 5 supernatant over a dark solid. Analysis of the product by GC indicated the following composition:

	<u>Component</u>	<u>GC Area %</u>
	CClF ₂ CF ₂ CClF ₂ /CCl ₂ FCF ₂ CF ₃	18.3
10	CCl ₃ CF ₃	55.1
	CF ₃ CCl ₂ CF ₂ CF ₂ CF ₃	0.3
	CF ₃ CF ₂ CCl ₂ CF ₂ CF ₃	21.2
	C ₃ Cl ₃ F ₅ isomers	2.1
	CCl ₄	0.7
15	C ₅ Cl ₃ F ₉ isomers	0.8

The modified aluminum chloride catalyst of Example 3 was prepared as follows:

- A 1 L four neck round bottom flask was charged with 150 g of aluminum chloride (AlCl₃) in a dry box. The flask was passed out of the dry box and fitted with an addition funnel, a mechanical stirrer, a thermocouple, and a dry ice condenser connected to a nitrogen bubbler. The addition funnel was charged with 410 g of CCl₃F and the condenser was filled with a methanol/dry ice mixture. The CCl₃F was added to the flask over the course of about 1 h. After the addition was complete, the mixture was stirred for 1 h and then volatiles were removed in vacuum. The resulting solid was dried under dynamic vacuum with gentle warming (70C water bath) to afford 120.6 g of pale yellow powder. Analysis: weight % Al = 25.5; this corresponds to a composition that is approximately AlCl_{1.3}F_{1.7}.

30 EXAMPLE 4

Reaction of CFC-12 with Tetrafluoroethylene

Example 3 was repeated with the exception that CHCl₂CF₃ was used as the diluent (120 g).

- After charging with CCl₂F₂, the cold reactor was placed in the barricade and charged with 15 g (0.15 mole) of TFE. The reactor was warmed to 29C over the course of 0.25 h and the pressure rose to 65 psig. TFE was then added to the reactor in 5 g increments at a temperature of 27-33C over the next 1.3 h until a total of 50 g (0.50 mole) had been added; the pressure gradually rose to 105 psig. The reactor was then held at a temperature 30-38C for 3 h; the final pressure was 58 psig. The following day the reactor was discharged to afford 205.4 g of a clear

- 5 supernatant over a dark solid. Analysis of the product by GC indicated the following composition:

	<u>Component</u>	<u>GC Area %</u>
	CClF ₂ CF ₂ ClF ₂ /CCl ₂ FCF ₂ CF ₃	20.6
10	CHCl ₂ CF ₃	59.3
	CF ₃ CCl ₂ CF ₂ CF ₂ CF ₃	0.2
	CF ₃ CF ₂ CCl ₂ CF ₂ CF ₃	16.8
	C ₃ Cl ₃ F ₅ isomers	1.8
	C ₅ Cl ₃ F ₉ isomers	0.7

15

EXAMPLE 5

Reaction of CFC-12 with Tetrafluoroethylene

- A 400 mL "Hastelloy" C shaker tube was charged with aluminum chloride (2 g, 0.015 mole). The reactor was sealed, cooled to -78C, evacuated,
 20 purged with nitrogen three times, and charged with CCl₂F₂ (50 g, 0.41 mole). The cold reactor was placed in the barricade and charged with 25 g (0.25 mole) of TFE. The reactor was warmed to 59C over the course of 0.3 h and the pressure rose to about 230 psig. The reactor was held at a temperature 52-60C for 3 h; the final pressure was 134 psig. The reactor was discharged to afford 41.1 g of a clear
 25 supernatant over a brown solid. Analysis of the product by GC/GC-MS indicated the following composition:

	<u>Component</u>	<u>GC Area %</u>
	CClF ₂ CF ₂ ClF ₂ /CCl ₂ FCF ₂ CF ₃	51.5
30	CF ₃ Cl ₂ CF ₂ CF ₂ CF ₃	0.5
	CF ₃ CF ₂ Cl ₂ CF ₂ CF ₃	14.8
	CCl ₃ C ₂ F ₅	22.0
	CCl ₂ FCF ₂ CClF ₂	5.4
	CClF ₂ CF ₂ CCl ₂ C ₂ F ₅	3.1
35	CCl ₂ =CCl ₂	0.8

- The formation of CCl₃C₂F₅ in such a substantial amount in the presence of initially unmodified AlCl₃, the amount being significantly greater than that produced in the presence of initially modified aluminum chloride catalyst
 40 (Examples 1-4), indicates disproportionation of CCl₂F₂ had occurred to CCl₃F

5 (among other products) followed by addition of CCl_3F to TFE. Further, it can be seen, in general, in comparison with the results of Examples 1-4, that the yields of the desired $\text{C}_3\text{Cl}_2\text{F}_6$ and $\text{C}_5\text{Cl}_2\text{F}_{10}$ products are lower than those obtained starting with an initially modified catalyst. The not insignificant yields of $\text{C}_3\text{Cl}_2\text{F}_6$ and $\text{C}_5\text{Cl}_2\text{F}_{10}$ products in Example 5 are believed the result of employing CCl_2F_2 in
 10 excess over the stoichiometric quantity.

EXAMPLE 6

Reaction of CCl_2F_2 with TFE - Continuous Process

A 1 L stainless steel, stirred autoclave was charged with 10 g of
 15 $\text{AlCl}_3\text{-xFx}$ modified aluminum chloride. The autoclave was sealed and evacuated and 100 g of CCl_3CF_3 were drawn into the autoclave under vacuum. At a temperature of 13°C and a pressure of 4 inches of vacuum, 20 g of TFE were fed to the autoclave. At an initial temperature and pressure of 10.9°C and 32.3 psig, TFE and CCl_2F_2 were then co-fed to the reactor at rates of 50 g/h and 37.5 g/h,
 20 respectively as the reactor temperature was brought to $30\text{-}31^\circ\text{C}$. Gas feeds was continued until the pressure reached 150 psig (31°C); 2.98 moles of TFE had been fed and 2.00 moles of CCl_2F_2 had been fed. After stirring for 3.5 h, the reaction was shut down and 502 g of product were discharged. GC analysis of the product indicated the following major products:

25	<u>Component</u>	<u>GC Area %</u>
	$\text{CCl}_2\text{F}_2\text{CF}_2\text{CCl}_2\text{F}_2/\text{CCl}_2\text{FCF}_2\text{CF}_3$	22.6
	$\text{CF}_3\text{CCl}_2\text{C}_2\text{F}_5$	1.8
	CCl_3CF_3	15.5
30	$\text{CF}_3\text{CCl}_2\text{CF}_2\text{CF}_2\text{CF}_3$	0.5
	$\text{CF}_3\text{CF}_2\text{CCl}_2\text{CF}_2\text{CF}_3$	52.0
	$\text{CCl}_3\text{C}_2\text{F}_5$	1.9
	$\text{CCl}_2\text{F}_2\text{CF}_2\text{CCl}_2\text{F}_2$	0.1
	CCl_4	2.4
35	$\text{C}_5\text{Cl}_3\text{F}_9$ isomers	1.3

The modified aluminum chloride catalyst used in this Example was prepared following a procedure similar to that described in Example 3. Analysis: weight % Al = 26.8; this corresponds to a composition that is approximately
 40 AlCl_1F_2 .

5

EXAMPLE 7Reaction of CCl_2F_2 with TFE - Continuous Process

A 1 L stainless steel, stirred autoclave was charged with 10 g of $\text{AlCl}_3 \cdot x\text{F}_x$. The autoclave was sealed and evacuated and 100 g of CCl_3CF_3 were drawn into the autoclave under vacuum. At a temperature of 16°C and a pressure of 2 inch of vacuum, TFE and CCl_2F_2 were co-fed to the autoclave at rates of 80 g/h and 97 g/h, respectively as the reactor temperature was brought to 31-34°C. Gas feeds were continued until the pressure reached 149 psig (31°C); 3.29 moles of TFE had been fed and 3.90 moles of CCl_2F_2 had been fed. After stirring for 2 h, the reaction was shut down and 551 g of product were discharged. GC analysis of the product indicated the following major products:

	<u>Components</u>	<u>GC Area %</u>
	$\text{CClF}_2\text{CF}_2\text{CClF}_2/\text{CCl}_2\text{FCF}_2\text{CF}_3$	30.2
20	$\text{CF}_3\text{CCl}_2\text{C}_2\text{F}_5$	0.3
	CCl_3CF_3	14.0
	$\text{CF}_3\text{CCl}_2\text{CF}_2\text{CF}_2\text{CF}_3$	0.6
	$\text{CF}_3\text{CF}_2\text{CCl}_2\text{CF}_2\text{CF}_3$	41.5
	$\text{CCl}_3\text{C}_2\text{F}_5$	7.7
25	$\text{CClF}_2\text{CF}_2\text{CCl}_2\text{F}$	0.8
	CCl_4	0.7
	$\text{C}_5\text{Cl}_3\text{F}_9$ isomers	2.9

The modified aluminum chloride catalyst used in this Example was prepared following a procedure similar to that described in Example 3. Analysis: weight % Al = 27.1; this corresponds to a composition that is approximately AlCl_1F_2 .

EXAMPLE 8Reaction of CBrClF_2 with Tetrafluoroethylene

A 400 mL "Hastelloy" C shaker tube was charged with CCl_3F -modified aluminum chloride (6.7 g). The tube was sealed, cooled to -78°C, evacuated, and purged with nitrogen three times. The reactor was then charged with CBrClF_2 (89.8 g, 0.54 mole). The cold reactor was placed in the barricade and charged with 42 g (0.42 mole) of TFE. The reactor was warmed to 40°C over the

5 course of 1 h during this period the pressure rose to 37 psig. The temperature was held at 40C for 1 h (pressure = 38 psig) and then raised to 80C and held for 2 h; during this time the pressure increased from 82 psig to 100 psig. The reaction was shut down at this point. The following day the reactor was discharged to afford 123.9 g of a orange supernatant over a dark solid. Analysis of the product by
 10 GC/GC-MS and ¹⁹F NMR indicated the following composition:

	<u>Component</u>	<u>GC Area %</u>	<u>Mole %</u>
	CCl ₂ F ₂	0.7	0.8
	CBrClF ₂	2.9	3.2
15	CBrClF ₂ CF ₂ CF ₃	54.0	39.9
	CBrF ₂ CF ₂ CClF ₂	*	19.1
	CCl ₃ CF ₂ CF ₃	0.4	0.3
	C ₅ BrClF ₁₀	0.4	
	C ₂ F ₅ CBrClCF ₂ CF ₃	27.2	24.8
20	C ₅ Br ₂ ClF ₉ (2)	0.8	
	CBr ₂ ClCF ₂ CF ₃	9.6	11.9
	C ₃ BrCl ₂ F ₅	1.6	-

*C₃BrCl₂F₆ isomers not separated by GC.

25 The modified aluminum chloride catalyst used in this Example was prepared following a procedure similar to that described in Example 1.

EXAMPLE 9

Reaction of CBrClF₂ with Tetrafluoroethylene

30 The procedure of Example 8 was repeated using 38 g of TFE (0.38 mole), 30 g of CBrClF₂ (0.18 mole), and 3 g of CCl₃F-modified aluminum chloride (see Example 1). The TFE was added portionwise at a maximum temperature of 36C (maximum pressure = 100 psig). The reaction was held at 36-39C for 1 h and then heated to 79-81C and held at that temperature for 2 h (final pressure = 118
 35 psig). The crude product weighed 58.3 g. Analysis of the product by GC and GC-MS indicated the following composition:

	<u>Component</u>	<u>GC Area %</u>
	CBrF ₂ CF ₂ CClF ₂	14.7
40	C ₅ BrClF ₁₀	1.7

5	C2F5CBrClC2F5	75.3
	C2F5CBr2C2F5	0.1
	C3Br2ClF5	1.3
	C5BrCl2F9	0.1
	C5Br2ClF9 (3)	0.9

10

EXAMPLES 10, 11, and 12

Reaction of CBr2F2 with TFE using a CCl3F-modified aluminum chloride catalyst

A 400 mL "Hastelloy" C shaker tube was charged with CCl3F-modified aluminum chloride (4 g) and CBr2F2 (63 g, 0.30 mole). The tube was sealed, cooled to -78C, evacuated, and purged with nitrogen three times. The cold reactor was placed in the barricade and charged with 30 g (0.30 mole) of TFE. The reactor was warmed to 100C over the course of 1 h during this period the pressure rose to 50 psig. The temperature was held at 99-101C for 4 h (max. pressure = 60 psig) and then heating and agitation were stopped. The following day the reactor was discharged to afford 91.6 g of a clear supernatant over a dark solid.

20

The reaction between CBr2F2 and TFE was repeated following the procedure above at a temperature of 60C (EXAMPLE 11) and at a temperature of 30C (EXAMPLE 12). The GC analyses of these runs are compared in the table below.

25

		Reaction Products, GC Area %		
	<u>Component</u>	<u>Ex. 10</u>	<u>Ex. 11</u>	<u>Ex. 12</u>
	CBrF2CF2CBrF2	14.0	13.7	13.7
	CBr2FCF2CF3	19.5	3.2	29.3
30	CBrCl2CF2CF3	0.2	0.2	0.3
	CF3CBr2CF2CF2CF3	6.2	8.5	0.8
	C2F5CBr2C2F5	34.4	57.4	39.7
	CBrF2CBr2CF3	19.0	6.3	2.2
	CBr3C2F5	0.4	0.06	8.0
35	C5Br3F9	1.2	1.2	2.1

The modified aluminum chloride catalyst used in Examples 10 and 11 were prepared following a procedure similar to that described in Example 1. Analysis: weight % Al = 27.7; this corresponds to a composition that is

- 5 approximately $\text{AlCl}_0.8\text{F}_2.2$. The modified aluminum chloride catalyst used in Example 12 was the same as that described in Example 1.

EXAMPLES 13 and 14

Reaction of CBr_2F_2 with TFE using a CCl_3F -modified Aluminum Chloride Catalyst

- 10 A 400 mL "Hastelloy" C shaker tube was charged with CCl_3F -modified aluminum chloride (see Example 1; 1 g) and CBr_2F_2 (42 g, 0.20 mole). The reactor was sealed, cooled to -78°C , evacuated, and purged with nitrogen three times. The cold reactor was placed in the barricade, agitation was begun, and 10 g (0.10 mole) of TFE were added. The reactor was warmed to 0°C over the course of 15 19 minutes; during this time the pressure decreased from 37 psig at -27°C to 22 psig at 0°C . An additional 17 g of TFE was added in five portions over the course of 1.2 h during which time the pressure rose to 61 psig. An additional 6 g of TFE were added bring the total pressure to 92 psig (total of 0.33 mole TFE added) and the reactor held at 30°C for 13 h (final pressure = 98 psig). Discharge of the reactor 20 afforded 61.1 g of a yellow supernatant over a brown solid.

The reaction of CBr_2F_2 with TFE was repeated (EXAMPLE 14) using 105 g (0.50 mole) of CBr_2F_2 and 40 g (0.40 mole) of TFE in the presence of 2 g of CCl_3F -modified aluminum chloride (see Example 1) at 30°C . The results of these two experiments are given in Table below.

25

Product Distribution for Reaction of TFE with 12B2

	Component	Ex. 13		Ex. 14	
		GC Area %	Mole %	GC Area %	Mole %
30	CBrF_3	0.08	-	0.5	1.2
	CBr_2F_2	0.8	-	0.9	1.3
	$\text{CBrF}_2\text{CF}_2\text{CBrF}_2$	12.8*	20.3	46.8*	24.0
	$\text{CBr}_2\text{FCF}_2\text{CF}_3$	1.5	-	*	31.5
	$\text{CF}_3\text{CBr}_2\text{CF}_3$	*	1.7	*	1.1
35	$\text{CF}_3\text{CBr}_2\text{CF}_2\text{C}_2\text{F}_5$	2.3	1.7	0.7	-
	$\text{C}_2\text{F}_5\text{CBr}_2\text{C}_2\text{F}_5$	72.6	69.2	29.0	23.3
	$\text{CBrF}_2\text{CBr}_2\text{CF}_3$	2.0	1.9	2.8	3.1
	$\text{CBr}_3\text{C}_2\text{F}_5$	2.4	2.8	14.3	14.6
	$\text{C}_2\text{F}_5\text{CBr}_2\text{CF}_2\text{CBrF}_2$	2.2	2.1	1.9	-
40	$\text{CBrF}_2\text{CF}_2\text{CBr}_3$	-	-	0.2	-

5

*GC trace did not separate C3Br2F6 isomers accurately.

EXAMPLE 15

Reaction of CBr2F2 with TFE

10 A 1 L stainless steel, stirred autoclave was charged with 10 g of CCl3F-modified aluminum chloride. The autoclave was sealed and evacuated and 500 g (2.38 moles) of chilled CBr2F2 were drawn into the autoclave under vacuum. TFE was fed to the autoclave at a rate of 2.2 g/min at an initial temperature and pressure of 23C and 1 psig, respectively; the temperature was brought to about 30C.
15 TFE feed was continued until the pressure reached 151 psig (29C). At this point the feed rate was decreased to 1.1 g/min. TFE was fed intermittently to the reactor keeping the pressure at a maximum value of 150 psig. The reaction was shut down after 4.76 moles of TFE had been fed to the reactor. Discharge of the reactor afforded 868 g of product. GC analysis of the product indicated the following major
20 products:

	<u>Component</u>	<u>GC Area %</u>
	C5BrF9 isomers	0.9
	CBrF2CF2CBrF2	13.5
25	CBr2FC2F5	6.3
	CBrCl2C2F5	0.8
	CF3CBr2CF2C2F5	4.2
	CF3CF2CBr2CF2CF3	63.1
	C3Br2ClF5 isomer	1.4
30	CBrF2CF2CBr2F	1.4
	CBr3C2F5	3.0
	C5Br3F9 isomers	2.1

35 The modified aluminum chloride catalyst used in this Example was prepared following a procedure similar to that described in Example 3. Analysis: weight % Al = 23.6; this corresponds to a composition that is approximately AlCl2F1.

EXAMPLE 16

40

Reaction of CBr2F2 with TFE using AlCl3 Catalyst

5 A 400 mL "Hastelloy" C shaker tube was charged with AlCl_3 (99.99%,
2 g, 0.015 mole) and sealed. The tube was cooled to -78°C , evacuated, and purged
with nitrogen three times. The cold reactor was then charged with CBr_2F_2 (63 g,
0.30 mole) and placed in the barricade. The reactor was agitated and then charged
with 10 g (0.10 mole) of TFE. The reactor was warmed to 31°C over the course of 40
10 minutes as the pressure rose to 94 psig. An additional 20 g of TFE were added in
three portions over the next 1.5 h. The temperature was held at $27\text{--}32^\circ\text{C}$; the
pressure was held at about 100 psig for most of this period, but rose to 162 psig as
the last few grams of TFE were added. The reactor was held at about 30°C for an
additional 6 h as the pressure dropped to 60 psig. The following day, the reactor
15 was discharged to afford 74.2 g of a clear supernatant over a brown solid. Analysis
of the product by GC and GC-MS indicated the following composition:

5	<u>Component</u>	<u>GC Area %</u>	<u>Mole %</u>
	CBrClF ₂	6.4	16.3
	CBrF ₂ CF ₂ CClF ₂	54.8	15.7
	CBrClFCF ₂ F ₅	*	41.5
	CF ₃ CBrClCF ₃	*	1.4
10	CCl ₃ CF ₂ CF ₃	1.7	1.6
	CCl ₂ FCF ₂ CClF ₂	0.4	-
	C ₅ BrClF ₁₀	0.4	-
	C ₂ F ₅ CBrClC ₂ F ₅	17.8	13.8
	CBrCl ₂ C ₂ F ₅	11.4	8.3
15	CBrF ₂ CF ₂ CCl ₂ F	-	1.3
	C ₂ F ₅ CBr ₂ C ₂ F ₅	0.07	-
	CBr ₂ ClC ₂ F ₅	3.2	-

*C₃BrClF₆ isomers not well separated on the GC column employed.

20

EXAMPLE 17

Reaction of CFC-12 with CTFE

A 400 mL "Hastelloy" C shaker tube was charged with 2 g of CCl₃F-modified aluminum chloride. The reactor was sealed, cooled in dry ice, evacuated and purged with nitrogen three times. The reactor was re-evacuated and charged
 25 with CFC-12 (50 g, 0.41 mole) and CTFE (35 g, 0.30 mole). The reactor was warmed to 30C and held at 30-39C for 8 h (max pressure, 160 psig at 38C; final pressure, 130 psig at 35C). The product (10.3 g) consisted of a small amount of yellow supernatant over a brown solid. Analysis of the product by GC, GC-MS, and 19F NMR indicated the following composition.

30

	<u>Component</u>	<u>GC Area %</u>	<u>Mole %</u>
	cyclo-cis-1,2-C ₄ Cl ₂ F ₆	23.1	21.1
	cyclo-trans-1,2-C ₄ Cl ₂ F ₆	34.2	28.7
	CClF ₂ CClFCClF ₂	1.1	4.0
35	CCl ₂ FCClFCF ₃	14.4	15.3
	CClF ₂ CF ₂ CCl ₂ F	7.4	11.0
	CCl ₃ C ₂ F ₅	*	0.4
	CClF ₂ CCl ₂ CF ₃	*	1.5
	C ₅ Cl ₄ F ₈ (3 isomers)	18.0	
40	CF ₃ CClFCCl ₂ CClFCF ₃		

5	(2 diastereomers)		4.5
	CClF ₂ CClFCF ₂ CCl ₂ CF ₃		7.8
	CClF ₂ CF ₂ CCl ₂ CF ₂ CClF ₂		4.2
	CCl ₃ CF ₂ CClF ₂	0.4	0.6
	CCl ₃ CClFCF ₃	0.6	0.7

10

The modified aluminum chloride catalyst used in this Example was prepared following a procedure similar to that described in Example 1. Analysis: weight % Al = 26.6; this corresponds to a composition that is approximately AlCl₁F₂.

15

EXAMPLE 18

Reaction of CBrClF₂ with CTFE

A 400 mL "Hastelloy" C shaker tube as charged with CCl₃F-modified aluminum chloride (6.7 g). The reactor was cooled to -78C, evacuated, and purged
 20 three times with nitrogen. CBrClF₂ (41 g, 0.25 mole) and CTFE (23 g, 0.20 mole) were sequentially condensed into the reactor. The cold reactor was placed in the barricade and agitation was begun. The reactor was heated to 40C and held for 3 h (50 psig) and then heated to 80C and held for 6 h. During the latter stage of the reaction the pressure increased from 80 to 90 psig. The product was discharged to
 25 give 55 g of a red-brown supernatant over a light-colored solid. Analysis of the product by GC, GC-MS, and ¹⁹F NMR indicated the composition listed below.

	<u>Component</u>	<u>GC Area %</u>	<u>Mole %</u>
	CF ₃ CBrClCClF ₂	34.8	48.5
30	CClF ₂ CF ₂ CBrClF	15.0	23.3
	CClF ₂ CClFCBrF ₂	*	10.4
	CCl ₂ FCF ₂ CBrClF	13.1	17.7
	CBrClF ₂	3.3	-
	CBrF ₂ CClF ₂	0.7	-
35	CBr ₂ F ₂	0.3	-
	C ₃ Cl ₂ F ₄	3.9	-
	CBrF ₂ CBrClF	0.5	-
	C ₅ Cl ₃ F ₇ (4)	3.8	-
	C ₄ BrCl ₄ F ₇	0.3	-
40	C ₃ BrCl ₂ F ₃ (2)	1.1	-

5

The modified aluminum chloride catalyst of Example 18 was prepared as follows:

10 A 2 L four neck creased round bottom flask was fitted with an addition funnel, a mechanical stirrer, a thermocouple, and a glycol/water-cooled condenser connected to a nitrogen bubbler. The flask was charged with 200 g of aluminum chloride (AlCl_3). CCl_3F (700 mL) was added to the flask over the course of about 1 h; during this time the temperature rose to about 67°C and gradually dropped to about 50°C. After the addition was complete, the mixture was stirred for 1 h. The supernatant was poured off and remaining volatiles were removed under 15 vacuum with gentle warming (70°C water bath) to afford 131 g of pale yellow powder. Analysis: weight % Al = 29.5; this corresponds to a composition that is approximately $\text{AlCl}_{0.5}\text{F}_{2.5}$.

EXAMPLE 19

20

Reaction of CBr_2F_2 with CTFE

A 400 mL "Hastelloy" C shaker tube was charged with CCl_3F -modified aluminum chloride (see Example 1; 3 g) and CBr_2F_2 (54 g, 0.26 mole). The tube was sealed, cooled to -78°C, evacuated, purged with nitrogen three times, and then charged with 29 g (0.25 mole) of CTFE. The cold reactor was placed in 25 the barricade and warmed to 30°C with agitation; the pressure rose to about 35 psig and then dropped to zero. The temperature was held at 29-35°C for 6 h. The following day the reactor was discharged to afford 60.7 g of a clear supernatant over a brown solid. Analysis of the product by GC and GC-MS indicated the following composition:

30

	<u>Component</u>	<u>GC Area %</u>
	$\text{CClF}=\text{CF}_2$	5.8
	$\text{CBrF}_2\text{CClF}_2$	1.7
	cyclo- $\text{C}_4\text{Cl}_2\text{F}_6$ (2)	11.7
35	$\text{C}_2\text{Br}_2\text{ClF}_3$	0.8
	$\text{C}_3\text{Br}_2\text{ClF}_5$	27.7
	$\text{C}_3\text{Br}_2\text{ClF}_5$	7.7
	$\text{C}_5\text{BrCl}_2\text{F}_7$	1.3
	$\text{C}_5\text{BrCl}_2\text{F}_7$	1.5
40	$\text{C}_5\text{BrCl}_2\text{F}_7$	1.4

5	C5BrCl2F7	1.1
	C3Br2ClF3	0.9
	C5Br2Cl2F8	2.0
	C5Br2Cl2F8	13.2
	C5Br2Cl2F8	3.6
10	C5Br2Cl2F8	17.6

EXAMPLE 20

Hydrogenation of CF₃CF₂CCl₂CF₂CF₃ over Pd/C Catalyst

A 15 inch (38.1 cm) x 3/8 inch (0.95 cm) "Hastelloy" nickel alloy tube was filled with 4.68 gm (about 13 mL) .5% Pd/C ground to 4/10 mesh. The catalyst was activated by heating at 120C for 135 min under a hydrogen flow of 50 sccm, 8.3x10⁻⁷ m³/s). The temperature of the reaction was raised to 175C while decreasing the flow of H₂ to 22 sccm (3.7x10⁻⁷ m³/s) and increasing the flow of CF₃CF₂CCl₂CF₂CF₃ to 7.3 sccm (1.2x10⁻⁷ m³/s). The gaseous effluent was found to be 93% CF₃CF₂CH₂CHF₂CF₃, an over hydrogenation product.

EXAMPLE 21

Hydrogenation of CF₃CF₂CCl₂CF₂CF₃ over Pd/C Catalyst

The reactor described in Example 20 was filled with 2.00 gm (about 6.0 cc) of .5% Pd/C ground to 4/10 mesh. The catalyst was activated by heating at 150C for 52 min. under a hydrogen flow of 50 sccm, 8.3x10⁻⁷ m³/s). The temperature of the reaction was lowered to 100C while decreasing the flow of H₂ to 3.8 sccm (6.3x10⁻⁸ m³/s) and increasing the flow of CF₃CF₂CCl₂CF₂CF₃ to 2.0 sccm (3.3x10⁻⁸ m³/s). The gaseous effluent was found to be 57% CF₃CF₂CH₂CHF₂CF₃, 9.4% CF₃CF₂CHClCF₂CF₃, 16% CF₃CF=CHCF₂CF₃, 4.8% CF₃CF₂CH₂CF₂CF₃, 2.8% CF₃CF=CClCF₂CF₃, 1.5% CF₃CHFCHClCF₂CF₃, as well as other unidentified by-products.

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EXAMPLE 22

Hydrogenation of CF₃CF₂CCl₂CF₂CF₃ over Pd/Al₂O₃ Catalyst

The reactor described in Example 20 was filled with 3.48 gm (about 6.0 cc) of .5% Pd/Al₂O₃ (Calsicat 1/8" pellets #64A-057) ground to 4/10 mesh. The catalyst was activated by heating at 100C for 50 min. under a hydrogen flow of 50 sccm, 8.3x10⁻⁷ m³/s). The temperature of the reaction was raised to 150C while decreasing the flow of H₂ to 20 sccm (3.3x10⁻⁷ m³/s) and increasing the flow of CF₃CF₂CCl₂CF₂CF₃ to 10.0 sccm (1.7x10⁻⁷ m³/s). The gaseous effluent was found to be 61% CF₃CF₂CHClCF₂CF₃, which can recycled, 25% CF₃CF₂CH₂CF₂CF₃, 3.1% CF₃CF=CClCF₂CF₃, <1% CF₃CHFCH₂CF₂CF₃,

While certain aspects of the invention have been described in particular detail a person in this art would recognize that other aspects and embodiments are encompassed by the appended claims.

10
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5 THE FOLLOWING IS CLAIMED:

1. A process for making perhalopropanes and/or pentanes which comprises:
 - (i) contacting
 - (a) a dihalodifluoromethane, $CXYF_2$, where X and Y are independently Cl or Br, with
 - 10 (b) a fluoroolefin which is at least one of tetrafluoroethylene and chlorotrifluoroethylene, in the presence of
 - (c) a modified aluminum chloride catalyst under addition condensation conditions to produce
 - (d) at least one of a perhalofluoropropane having 5 to 6 fluorine and 2 to
15 3 nonfluorohalogen substituents totalling 8 halogens and
 - (e) a perhalofluoropentane having 8 to 10 fluorine and 2
to 4 nonfluorohalogen substituents totalling 12 halogen substituents,
the fluorine content of said propanes and pentanes being the sum of
the fluorine contents of the (a) and (b) reactants; and
 - 20 (ii) recovering at least one of said perhalopropanes and pentanes.
2. The process of Claim 1 wherein the modified catalyst is produced before said catalyst is contacted with said reactants.
- 25 3. The process of Claim 1 wherein the modified catalyst is produced in situ.
4. The process of Claim 1 wherein the fluoroolefin comprises TFE, the propane when produced has the formula C_3XYF_6 , and the pentane when
30 produced has the formula C_5XYF_{10} .
5. The process of Claim 1 wherein the $CXYF_2$ reactant comprises CCl_2F_2 and at least one propane when produced has the formula $C_3Cl_2F_6$, and at least one pentane when produced has the formula $C_5Cl_2F_{10}$.
35
6. The process of Claim 5 wherein said $C_3Cl_2F_6$ comprises one or more of $CCl_2FCF_2CF_3$ and $CClF_2CCF_2CClF_2$; and said $C_5Cl_2F_{10}$ comprises one or more of $C_2F_5CCl_2C_2F_5$ and $CF_3CCl_2CF_2CF_2CF_3$.

5 7. The process of Claim 1 wherein the CXYF₂ comprises CBrClF₂ and said perhalofluoropropane and perhalofluoropentane comprise one or more isomers having the formula C₃BrClF₆ and C₅BrClF₁₀.

10 8. The process of Claim 8 wherein the propane isomers comprise at least one member from the group consisting of CBrF₂CF₂CClF₂, CBrClFC₂F₅, CF₃CBrFCClF₂, and CF₃CBrClCF₃, and the pentane isomers comprise at least one member from the group consisting of C₂F₅CBrClC₂F₅, and CF₃CBrClCF₂CF₂CF₃.

15 9. The process of Claim 1 wherein the CXYF₂ reactant comprises CBr₂F₂, and the reaction product mixture comprises at least one of a perbromofluoropropane and a perbromofluoropentane, wherein the perbromofluoropropane comprises one or more isomers having the formula C₃Br₂F₆ and the perbromofluoropentane comprises one or more isomers having
20 the formula C₅Br₂F₁₀.

 10. The process of Claim 9 wherein the propane isomers comprise at least one of CBrF₂CF₂CBrF₂ and CBr₂FC₂F₅, and the pentane isomers comprise at least one of C₂F₅CBr₂C₂F₅ and CF₃CBr₂CF₂CF₂CF₃.

25 11. The process of Claim 1 wherein the CXYF₂ reactant comprises CBr₂F₂, the catalyst comprises aluminum chloride, and the reaction mixture comprises at least one of perhalofluoropropane having the formula C₃BrClF₆ and a perhalofluoropentane having the formula C₅BrClF₁₀.

30 12. The process of Claim 11 wherein the C₃BrClF₆ comprises one or more of CBrF₂CF₂CClF₂, CBrClFC₂F₅, and CF₃CBrClCF₃; and the C₅BrClF₁₀ comprises C₂F₅CBrClC₂F₅.

35 13. The process of Claim 1 wherein the fluoroolefin reactant comprises CTFE, and the propane product has the formula C₃ClX₂YF₅, and the pentane product having 8 fluorine and 4 nonfluorohalogen substituents has the formula C₅Cl₂X₂YF₈.

5 14. The process of Claim 13 wherein the CXYF₂ reactant comprises CCl₂F₂, the propane reaction product comprises C₃Cl₃F₅, and the pentane reaction product comprises C₅Cl₄F₈.

10 15. The process of Claim 14 wherein the C₃Cl₃F₅ product comprises one or more of CCIF₂CCIFCCIF₂, CCl₂FCCIFCF₃, CCl₂FCF₂CCIF₂, and CCl₃CF₂CF₃; and the C₅Cl₄F₈ reaction product comprises one or more of CF₃CCIFCCl₂CCIFCF₃, CCIF₂CCIFCF₂CCl₂CF₃, and CCIF₂CF₂CCl₂CF₂CCIF₂.

15 16. The process of Claim 1 wherein the CXYF₂ reactant comprises CBrClF₂, the propane reaction product comprises C₃BrCl₂F₅ and the pentane reaction product comprises C₅BrCl₃F₈.

20 17. The process of Claim 16 wherein the C₃BrCl₂F₅ comprises one or more of CBrF₂CCIFCCIF₂, CBrClFCF₂CCIF₂, and CF₃CBrClCCIF₂.

25 18. The process of Claim 14 wherein the CXYF₂ reactant comprises CBr₂F₂, the propane reaction product comprises C₃Br₂ClF₅ and the pentane reaction product comprises C₅Br₂Cl₂F₈.

 19. The process of Claim 18 wherein the C₃Br₂ClF₅ propane reaction product comprises one or more of CBr₂FCCIFCF₃ and CBr₂FCF₂CCIF₂, and C₅Br₂Cl₂F₈.

30 20. A composition of matter comprising at least one of a perhalofluoropropane and a perhalofluoropentane, the propane having 5 to 6 fluorine, 2 to 3 nonfluorohalogen substituents at least one of which is bromine and a total of 8 halogens, the pentane having 8 to 10 fluorines, 2 to 4 nonfluorine halogen substituents, at least one of which is bromine and a total of 10 halogens.

35 21. The composition of Claim 20 wherein the composition comprises at least one member from the group consisting of CCIF₂CF₂CBrClF, CBrCl₂CF₂CF₃ and CBrF₂CF₂CCl₂F; CBr₃CF₂CF₃ and CBrF₂CBr₂CF₃; CCIF₂CCIFCF₂CCl₂CF₃ and CCIF₂CF₂CCl₂CF₂CCIF₂; C₅Br₂Cl₂F₈ isomers; 40 CCIF₂CF₂CCl₂CF₂CF₃, C₅BrCl₂F₉ isomers; C₅Br₂ClF₉ isomers;

- 5 CBrF₂CF₂CBr₂CF₂CF₃; C₂F₅CCl₂C₂F₅ and CF₃CCl₂CF₂CF₂CF₃;
C₂F₅CBrClC₂F₅ and CF₃CBrClCF₂CF₂CF₃; C₂F₅CBr₂C₂F₅ and
CF₃CBr₂CF₂CF₂CF₃.

10 22. A process for hydrogenating the recovered perhalofluoropropanes
or pentanes of Claim 1 which process comprises:

- 15 (i) contacting at least one of said propane and pentane with molecular
hydrogen in the presence of a Group VIII metal hydrogenation
catalyst at a temperature and pressure effective to result in the
replacement of at least one nonfluorohalogen substituent with a
hydrogen substituent, thereby forming a hydrogenated propane or
pentane containing at least one more hydrogen substituent and at
least one less nonfluorohalogen substituent, and
20 (ii) recovering said hydrogenated propane or pentane.

20 23. The process of Claim 22 wherein said contacting of step (i) is
carried out in the vapor phase over a palladium catalyst.

25 24. The process of Claim 22 wherein the palladium is supported on
carbon or alumina.

25 25. The process of Claim 24 wherein the support comprises alumina.

A. CLASSIFICATION OF SUBJECT MATTER

IPC 6 C07C17/278 C07C19/10 C07C19/14 C07C17/23

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 6 C07C

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

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Y	US,A,5 220 084 (K. OHNISHI ET AL.) 15 June 1993 see column 8 - column 9; example 12 --- -/--	1

☒ Further documents are listed in the continuation of box C.☒ Patent family members are listed in annex.

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Date of the actual completion of the international search

11 April 1995

Date of mailing of the international search report

26. 04. 95

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INTERNATIONAL SEARCH REPORT

International Application No

PCT/US 94/14367

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
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